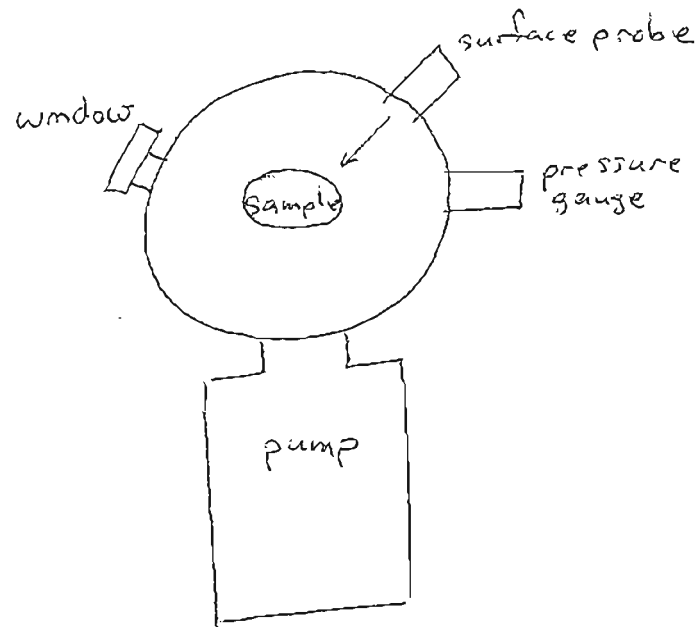


Surface Analysis \Rightarrow Need for Vacuum Technology



Different Types of Pumps

Different Types of Gauges

Different Types of Vacuum Chambers / Fittings

Advances in Vacuum Technology

Different Types of Pumps

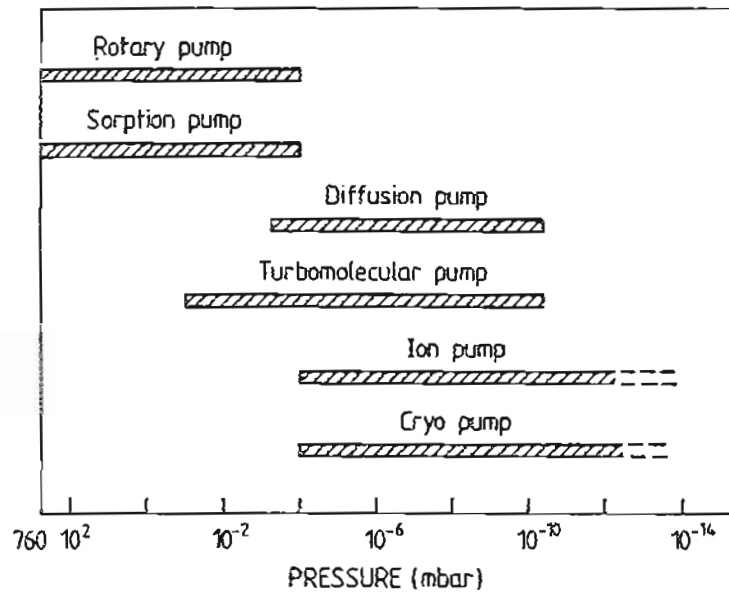


Fig. I.2. Pressure ranges in which different types of pumps can be employed

- H. Lüth, p. 7
Surfaces and Interfaces
of Solid Meth

The Pumping Equation

Particle number rate of change = $\frac{dN}{dt}$

$$\frac{dN}{dt} = \text{rate in} - \text{rate out}$$

$$\frac{dN}{dt} = \frac{dN_{in}}{dt} - \frac{dN_{out}}{dt}$$

$\frac{dN_{in}}{dt} =$ particle flux from vessel walls \times wall area

$$\frac{dN_{in}}{dt} = v A_w$$

$\frac{dN_{out}}{dt} =$ rate of particles being pumped out

$$PV = NkT$$

constant pressure

$$P \frac{dV}{dt} = \frac{dN_{out}}{dt} kT$$

$$\frac{dV}{dt} = S$$

$$\Rightarrow \frac{dN_{out}}{dt} = \frac{PS}{kT}$$

$$\Rightarrow \frac{dN}{dt} = v A_w - \frac{PS}{kT}$$

$$\Rightarrow v A_w = \frac{dN}{dt} + \frac{PS}{kT}$$

$$PV = NkT$$

constant volume

$$\frac{dp}{dt} \frac{V}{kT} = \frac{dN}{dt}$$

$$\Rightarrow v A_w = \frac{dp}{dt} \frac{V}{kT} + \frac{PS}{kT}$$

$$v A_w = \frac{V}{kT} \left(\frac{dp}{dt} + \frac{PS}{V} \right)$$

constant volume equation

$$g A_w = V \frac{dp}{dt} + PS$$

$$g A_w = Q + PS$$

$$kT \frac{dN}{dt} = (kTv) A_w - PS$$

$$= \frac{d(NkT)}{dt} = \frac{d(PV)}{dt} = Q$$

$Q \equiv$ throughput

$$g = kTv$$

~~more general formula~~

$$\Rightarrow Q = g A_w - PS$$

more general formula

Example 1:

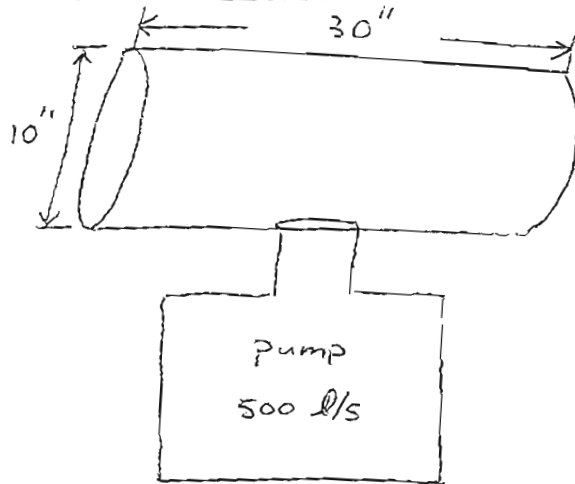
Suppose constant pressure $\frac{dp}{dt} = 0$

$$\Rightarrow vA_v = \frac{\rho S}{kT}$$

here Q is zero

$$\Rightarrow \boxed{p = \frac{kT}{S} vA_v = \frac{\rho A_v}{S}} \quad q \equiv kTv$$

$$\text{Area} = \pi(5'')^2 \left(\frac{0.0254\text{m}}{''} \right)^2 (2) + 2\pi(5'') \left(\frac{0.0254\text{m}}{''} \right)^2 (30'')$$



$$A_v = .709 \text{ m}^2$$

q for baked stainless steel

$$q = 400 \times 10^{-11} \text{ W/m}^2$$

~~$$S = \frac{q A_v}{p} = \frac{400 \times 10^{-11} \text{ W/m}^2 \cdot .709 \text{ m}^2}{5.67 \times 10^{-9} \text{ Pa}} = 4.61 \times 10^{-3} \text{ m}^3/\text{s}$$~~

$$S = 500 \text{ l/s} = .5 \text{ m}^3/\text{s}$$

$$\Rightarrow p = \frac{400 \times 10^{-11} \text{ W/m}^2 \cdot .709 \text{ m}^2}{(.500 \text{ m}^3/\text{s})} (400 \times 10^{-11} \text{ W/m}^2) (.709 \text{ m}^2)$$

$$p = 5.67 \times 10^{-9} \text{ Pa}$$

$$1 \text{ atm} = 760 \text{ torr} = 10^5 \text{ Pa}$$

\Rightarrow

$$p = 5.67 \times 10^{-9} \text{ Pa} \left(\frac{760 \text{ torr}}{10^5 \text{ Pa}} \right)$$

$$p = 4.3 \times 10^{-11} \text{ torr}$$

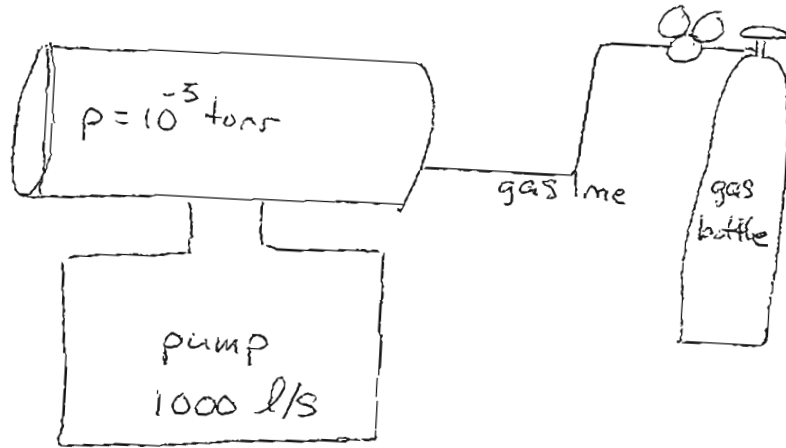
a very respectable pressure

Example 2

Gas flow Conditions

~~1000000~~

Question:
What is the "flow rate" of gas in the gas line in sccm?



1 sccm \equiv 1 standard cubic centimeter per minute

In this case,

$$pA_0 \ll pS$$

$$\Rightarrow |Q| = pS = \text{throughput} = 4T \frac{dN}{dt}$$

Key Point is constant throughput

$$\Rightarrow pS|_{\text{chamber}} = pS|_{\text{gasline}}$$

$$\frac{(10^{-5} \text{ torr})(1000 \text{ l/s})}{(760 \text{ torr})} = S$$

1 atm

$$S = 1.32 \times 10^{-2} \text{ scc/s}$$

$$S = .79 \text{ sccm}$$

standard cubic cm
per minute

Example 3

Suppose there exists a leak in the chamber at a rate of particles per second of L

$$vA_0 \rightarrow vA_0 + L$$

Assuming $L \gg vA_0$ and constant volume
(of chamber)

$$\Rightarrow L = \frac{V}{kT} \left(\frac{dp}{dt} + \frac{pS}{V} \right)$$

To determine the leak rate, one could turn off the pump $\Rightarrow S \rightarrow 0$

$$\text{Then } L = \frac{V}{kT} \frac{dp}{dt}$$

$$q_L = kTL = V \frac{dp}{dt}$$

measuring dp/dt with a pressure gauge,

q_L is calculated

Modification of Equations for Pump tubing

must consider conductance C

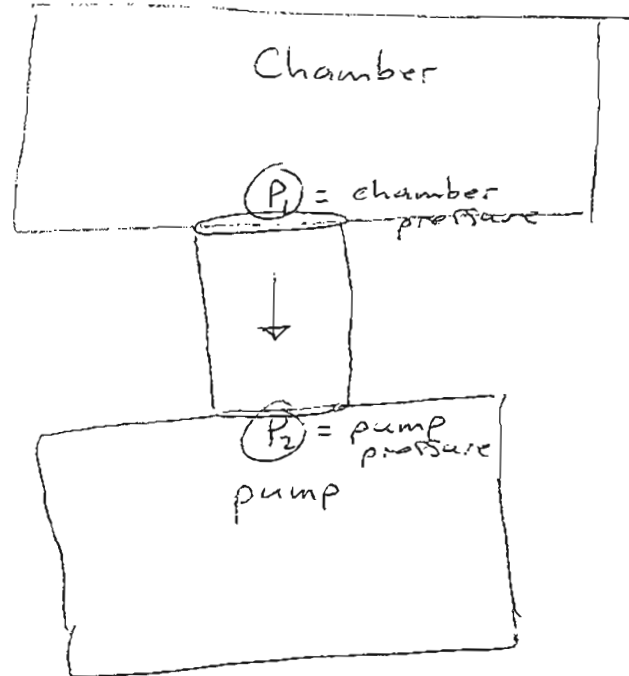
$$C = \frac{\text{throughput}}{\text{pressure difference}}$$

$$C = \frac{Q}{\Delta P}$$

or $Q = C \Delta P$

$$hT \frac{dN}{dt} = C \Delta P$$

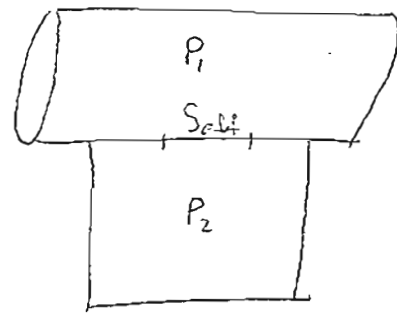
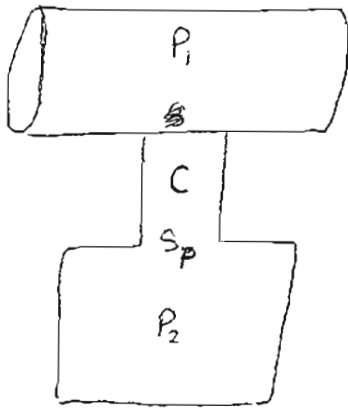
$$\frac{dN}{dt} = \frac{C \Delta P}{hT}$$



Key Point is that any pipe or tube has a conductance which depends on the pressure.

The finite conductance always limits the effective pumping speed.

Effective Pumping Speed



Assume at the pump entrance, $Q = pS$
($Q \gg SA$)

$$P_2 = \frac{Q}{S_p}$$

$$P_1 = \frac{Q}{S_{eff}}$$

By definition,

$$\frac{Q}{C} = \Delta P = P_1 - P_2$$

$$\Rightarrow P_1 = P_2 + \frac{Q}{C} = \frac{Q}{S_p} + \frac{Q}{C} = \frac{Q}{S_{eff}}$$

$$\Rightarrow \boxed{\frac{1}{S_{eff}} = \frac{1}{S_p} + \frac{1}{C}}$$

Similar to an electrical circuit

Conductances in parallel (parallel tubes)

have:

$$C_T = C_1 + C_2 + \dots$$

Conductances in series (series tubes)

have:

$$\frac{1}{C_T} = \frac{1}{C_1} + \frac{1}{C_2} + \dots$$

Different Flow Regimes

1. Viscous flow (higher pressures) ($pd > 10 \text{ mbar} \cdot \text{mm}$)

$$\sim 10 \text{ torr mm}$$

$$\sim 0.4 \text{ torr mch}$$

\Rightarrow • mean free path of molecule
less than pipe dimensions

• molecule - molecule collisions important

$$C \text{ [l/s]} = 137 \frac{d^4 \text{ [cm}^4\text{]} p \text{ [mbar]}}{L \text{ [cm]}}$$

2. molecular flow (low pressure) ($pd < 0.1 \text{ mbar} \cdot \text{mm}$)

\Rightarrow • mean free path of molecule greater
than pipe dimensions

• molecule - wall collisions important

$$C \text{ [l/s]} = 12 \frac{d^3 \text{ [cm}^3\text{]}}{L \text{ [cm]}}$$

viscous

$$d = 10 \text{ cm } L = 100 \text{ cm}, p = \frac{1}{10} \text{ mbar}$$

$$\Rightarrow C = \text{~~13700~~ } 13700 \text{ l/s}$$

molecular

$$C = 120 \text{ l/s}$$